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Pyrolysis characteristics of cathode from spent lithium-ion batteries using advanced TG-FTIR-GC/MS analysis

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Abstract

Thermal treatment offers an alternative method for the separation of Al foil and cathode materials during spent lithium-ion batteries (LIBs) recycling. In this work, the pyrolysis behavior of cathode from spent LIBs was investigated using advanced thermogravimetric Fourier transformed infrared spectroscopy coupled with gas chromatography-mass spectrometer (TG-FTIR-GC/MS) method. The fate of fluorine present in spent batteries was probed as well. TG analysis showed that the cathode decomposition displayed a three-stage process. The temperatures of maximum mass loss rate were located at 470 °C and 599 °C, respectively. FTIR analysis revealed that the release of CO₂ increased as the temperature rose from 195 to 928 °C. However, the evolution of H₂O showed a decreasing trend when the temperature increased to above 599 °C. The release of fluoride derivatives also exhibited a decreasing trend, and they were not detected after temperatures increasing to above 470 °C. GC-MS analysis indicated that the release of H₂O and CO displayed a similar trend, with larger releasing intensity at the first two stages. The evolution of 1,4-difluorobenzene and 1,3,5-trifluorobenzene also displayed a similar trend—larger releasing intensity at the first two stages. However, the release of CO₂ showed a different trend, with the largest release intensity at the third stage, as did the release of 1,2,4-trifluorobenzene, with the release mainly focused at the temperature of 300–400 °C. The release intensities of 1,2,4-trifluorobenzene and 1,3,5-trifluorobenzene were comparable, although smaller than that of 1,4-difluorobenzene. This study will offer practical support for the large-scale recycling of spent LIBs.

Keywords Electronic waste · Lithium-ion batteries · Cathode · Pyrolysis · Polyvinylidene fluoride binder

Introduction

The rapid growth in the production and consumption of lithium-ion batteries (LIBs) for portable electronic devices and electric vehicles has resulted in a large quantity of spent

LIBs (Sun et al. 2018; Tran et al. 2019; Wang et al. 2019a; Xiao et al. 2020; Zeng and Li 2014). More than 11 million tonnes of spent LIB packs are expected to be discarded by 2030, worldwide—500,000 metric tonnes from China alone, by 2020. As we all know, a considerable portion of valuable

metals, such as Li, Co, Cu, and Al are reserved within these spent LIBs. In view of their negative effects of spent LIBs on the environment and the considerable amounts of valuable metals reserved in them, it is highly desirable and beneficial to recycle this waste (Winslow et al. 2018; Zhang et al. 2018d). However, such recycling is still a challenge, and only about 5% of the spent LIBs are in fact recycled (Natarajan and Aravindan 2018). Recently, many advanced technologies, such as hydrometallurgy, pyrometallurgy, and bio-metallurgy, have been developed for recycling spent LIBs (Liu et al. 2019; Zhang et al. 2018c; Zhao et al. 2019). Carbon black contained in spent LIBs can be separated through mechanical treatment because of the low adhesion between carbon black and copper foil. However, the Al foil and cathode materials are difficult to separate because they are firmly adhered by polyvinylidene

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fluoride (*PVDF*) binder (Wang et al. 2019b; Zeng and Li 2014; Zhang et al. 2018a). A common method of detaching cathode materials from Al foil consists of dissolving Al foil with acidic or alkaline solutions (Chen and Zhou 2014; Gao et al. 2018). The dissolved metals can be further refined by extraction or precipitation processes. However, refractory wastewater will be generated by this method. *PVDF* can be dissolved using organic solvents (e.g., ionic liquid, *N*-methyl-2-pyrrolidone, *N,N*-dimethylformamide) according to the “like dissolves like” rule (Duan et al. 2018; Natarajan and Aravindan 2018; Zeng and Li 2014). This method is efficient,

but the use of volatile or expensive solvents will not only increase the recycling cost but also pose a risk to workers in the recycling facilities. *PVDF* can also be partially ruptured by oxidants, such as Fenton reagents (He et al. 2017). However, wastewater containing impurity ions will be generated as well. Decomposing *PVDF* using thermal treatment offers advantages of high efficiency and simple operation (Cheng et al. 2019; Qi et al. 2019; Wang et al. 2018). Wang et al. (2019b) used molten salt technology to decompose *PVDF*. The maximum detaching rate of cathode material reached 99.8 wt. %.

Zhang et al. (2018a, 2018b, 2018c, 2019) and Wang et al. (2018) applied pyrolysis treatment to remove *PVDF*. The recovery rate of cathode materials reached 98.23% under optimal conditions. Xiao et al. (2017) used vacuum pyrolysis to treat cathode material, and lithium carbonate was recovered, although it is worth noting that the fluorine present in *PVDF* could be transformed and transmitted into off-gas during thermal treatment of spent LIBs, causing reactor corrosion and air pollution. Nevertheless, this method is worth studying, even though few researches have focused on it. Therefore, in this work, we investigated it, considering not only the thermal behaviors of the cathode materials but also the fate of fluorine. It is expected that our results will offer practical support for the large-scale recycling of spent LIBs.

Materials and methods

Materials

The spent LIBs were collected locally from mobile phone service providers. Prior to usage, they were discharged using NaCl solution to mitigate the potential risk of short circuiting or LIBs blasts. After drying, the discharged batteries were dismantled manually, and the metallic shell, organic separators, cathode, and anode were separated. The recovered cathodes were crushed and used as raw material for the experiments. In this study, the binding agent used for cathode was *PVDF*. During the LIBs preparation, *PVDF*, conductive agent acetylene black, and lithium cobalt oxide were generally stirred and mixed in a solvent *N*-methyl-2-pyrrolidone to form a uniform positive electrode slurry. The slurry was coated on a

positive electrode current collector aluminum foil and dried and cold pressed to obtain a positive electrode plate.

Experimental methods

The online testing of evolved products during cathode thermal pretreatment was performed using a TG-FTIR-GC/MS (TGIRGCMS*/TGA8000*, PerkinElmer) coupled system. During analysis, approximately 2 mg of samples was heated from 30 to 1000 °C at a heating rate of 15 K min⁻¹ with a flow rate of 50 mL min⁻¹ for helium. Each test was repeated three times. The coupling systems between TG-FTIR-GC/MS were heated to prevent the condensation of volatile products.

Results and discussion

TG analysis

The thermogravimetric (TG) and derivative thermogravimetric (DTG) profiles of the cathode materials are displayed in Fig. 1. It can be seen that the cathode decomposition displayed a three-stage process, consistent with the previous reports (Zhang et al. 2014; Zhang et al. 2018a; Zhang et al. 2018b). There were two significant mass losses of 0.69% and 1.64% throughout the temperature ranges of 30–487 °C and 30–628 °C, respectively. The temperatures of maximum mass loss rate were determined as 470 °C and 599 °C, respectively. The mass loss in the initial stage was mainly attributed to the decomposition of *PVDF*, which was comparable to the reported decomposition temperature of 450–550 °C (Cao et al. 2016; Kar et al. 2015; Ma et al. 2012; Ouyang et al. 2015; Rathore et al. 2019). The loss in the second stage was mainly caused by the acetylene black oxidization (Cho et al. 2013; Nie et al. 2015). Cho et al. (2013) reported an exothermic peak of 604 °C for acetylene black decomposition. The loss in the last stage was attributed to the decomposition of lithium cobalt oxide (Antolini and Ferretti 1995; Zhang et al. 2014). From

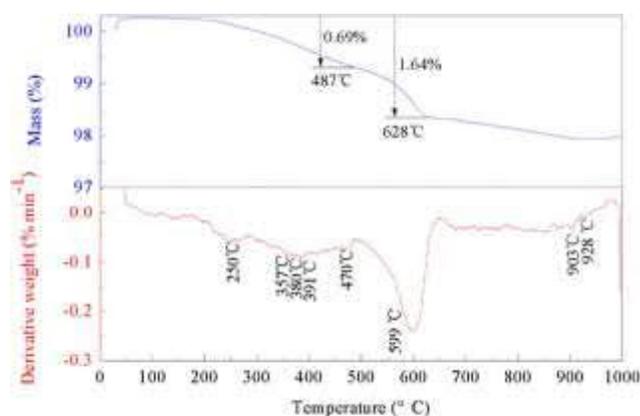


Fig. 1 TG-DTG profiles of cathode thermal treatment

the TG-DTG profiles, the optimal temperature for detaching cathode from Al foil was found to be approximately 650 °C.

Fourier transform infrared analysis

The 3D Fourier transform infrared (FTIR) spectra of the gas phase during the decomposition of cathode material are shown in Fig. 2. According to the y-axis (temperature) and z-axis (absorbance), the cathode decomposed vigorously, and more gaseous products were released in the temperature range of 550–1000 °C. From the perspective of the x-axis (wavenumbers) and the z-axis (absorbance), it can be observed that the absorbance peaks of evolved products were mainly located at 2000–2500 cm^{-1} (confirmed by Fig. 3). In addition, minor absorbances at 1500–2000 cm^{-1} and 3500–4000 cm^{-1} were also detected.

In order to probe the evolution of volatilized products, major signals from the gas phase spectra changes with respect to temperature were separated from the 3D spectra. In Fig. 4, the major peaks at 669, 2322, and 2360 cm^{-1} were attributed to the C–O bonds from CO_2 (Escribano et al. 2013; Yao et al. 2018; Yu et al. 2019). Minor peaks located at 1340 cm^{-1} were attributed to the C–F stretching vibration (Danilich et al. 1995; Mann et al. 1954). The bands at 1510 and 3739 cm^{-1} corresponded to the bending mode of H_2O . The release of CO_2 increased as temperatures increased from 195 to 928 °C. However, the release of H_2O showed a decreasing trend when the temperature increased to above 599 °C. The release of fluoride derivatives also exhibited a decreasing trend. They were not detected after temperatures increased to above 470 °C.

MS analysis

The simultaneous evolution of several volatile compounds having similar chemical structures did not allow the

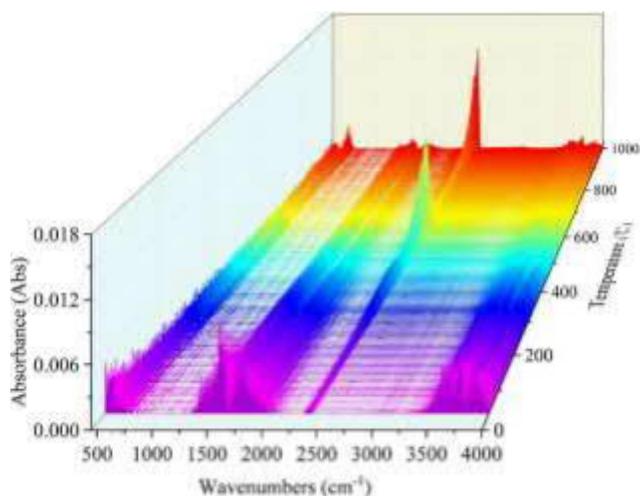


Fig. 2 3D infrared spectrum of evolved products for cathode thermal treatment

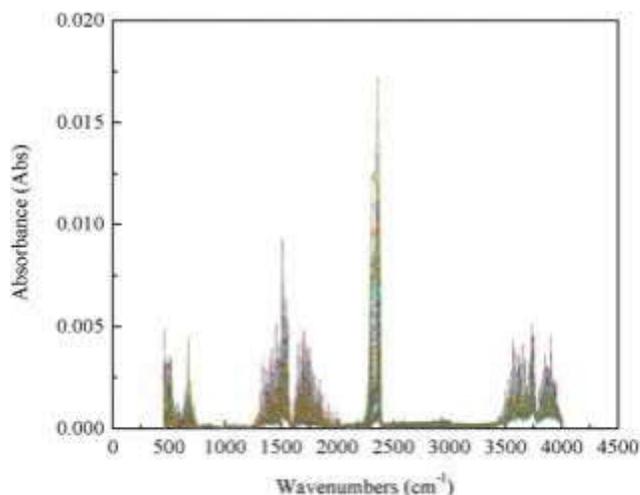


Fig. 3 2D infrared spectrum of evolved products for cathode thermal treatment

identification of single species by FTIR analysis, and thus MS analysis was adopted, to ensure the identification of specific products (Kai et al. 2017). First, a preliminary scan was carried out to identify the prominent ions with m/z in the range of 18 to 132 (see Fig. 5). Then, the main ionized fragments were tracked using multiple ion detection (MID) mode. Signals from m/z 12, 28, 44, 114, and 132 accounted for the evolution of small molecules H_2O , CO , CO_2 , difluorobenzene ($\text{C}_6\text{H}_4\text{F}_2$, DFB), and trifluorobenzene ($\text{C}_6\text{H}_3\text{F}_3$, TFB), respectively. Consistent with the DTG results, more gaseous products evolved in the temperature range of 350–650 °C. Signals at m/z 18, 28, and 44 revealed that the release of H_2O , CO , and CO_2 showed a three-stage process in the temperature ranges of 300–500 °C, 500–700 °C, and 700–900 °C, respectively. The release of H_2O and CO displayed a similar trend, with larger releasing intensity at the first two stages. However, the evolution of CO_2 showed a distinctive trend, with the largest release

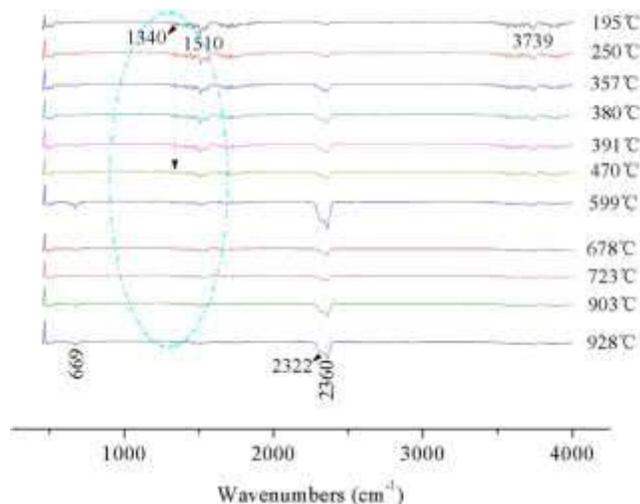
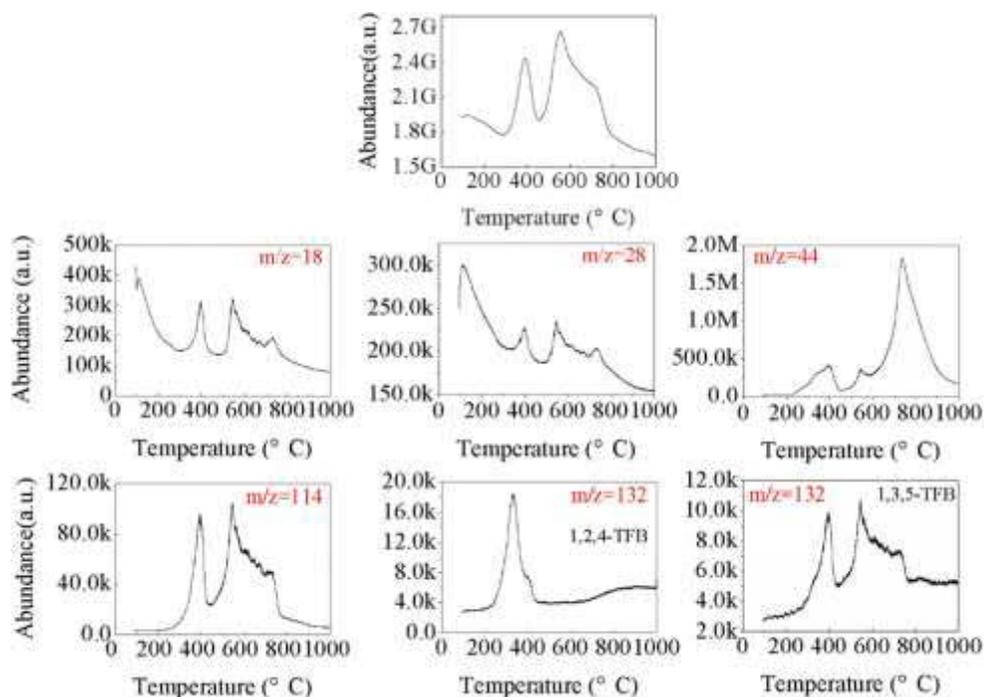


Fig. 4 FTIR spectra of volatilized products in cathode material thermal treatment

Fig. 5 Ion abundance distributions of evolved products along with temperatures



intensity at the third stage. Its release intensity was also larger than that of either H₂O or CO. This was consistent with the FTIR analysis in Fig. 4. In addition, fluorinated derivatives from the decomposition of PVDF were also detected, which was consistent with the FTIR analysis. Ion signals from m/z 114 and 132 indicated the evolution of 1,4-difluorobenzene (C₆H₄F₂, 1,4-DFB), 1,2,4-trifluorobenzene (1,2,4-TFB), and 1,3,5-trifluorobenzene (1,3,5-TFB). The release of 1,4-DFB and 1,3,5-TFB displayed a similar trend, with larger releasing intensity at the first two stages. However, the release of 1,2,4-TFB showed a different trend, with the release mainly focused at the temperature range of 300–400 °C. The release intensities of 1,2,4-TFB and 1,3,5-TFB were comparable, although smaller than that of 1,4-DFB. The occurrence of fluorinated derivatives, such as 1,4-DFB, 1,2,4-TFB, and 1,3,5-TFB, were also detected in the pyrolysis of pure PVDF, although they were not identical due to differences in the temperature and sample characteristics. Choi and Kim (2012) revealed that the major products of PVDF pyrolysis were vinylidene fluoride (VDF), 1,3,5-TFB, 1,4-DFB, 1,2,4-TFB, and 1,3,3,5,5-pentafluorocyclohexene. O'Shea et al. (1990) reported that increasing pyrolysis temperature resulted in a complex degradation process and a pyrolytic residue made up of largely aliphatic and fluoroaromatic structures. The report of Zulfiqar et al. (1994) also indicated that the major degraded products of PVDF were HF, VDF, and C₄H₃F₃.

Conclusions

The thermogravimetric analysis indicated that the cathode decomposition displayed a three-stage process. There were two significant mass losses of 0.69% and 1.64% throughout the temperature ranges of 30–487 °C and 30–628 °C, respectively, and the temperatures of maximum mass loss rate were located at 470 °C and 599 °C, respectively. The FTIR analysis indicated that the release of CO₂ increased as temperatures rose from 195 to 928 °C. However, the release of H₂O showed a decreasing trend when the temperature increased to above 599 °C. The release of fluoride derivatives also exhibited a decreasing trend, and they were not detected after temperatures increased to above 470 °C. The GC-MS analysis revealed that more gaseous products were evolved in the temperature range of 350–650 °C. The release of H₂O and CO displayed a similar trend, with larger releasing intensity at the first two stages. However, the evolution of CO₂ showed a distinctive trend, with the largest release intensity at the third stage. Its release intensity was also larger than that of H₂O or CO. The release of 1,4-DFB and 1,3,5-TFB displayed a similar trend, with larger releasing intensity at the first two stages. However, the release of 1,2,4-TFB showed a different trend, and the release was mainly focused at the temperature range of 300–400 °C. The release intensities of 1,2,4-TFB and 1,3,5-TFB were comparable, although smaller than that of 1,4-DFB.

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